

Monday, December 28, 2020

Net Positive Suction Head (NPSH) Part 4 of 5 – Gauge Readings

Monday Morning Minutes | by Norm Hall, December 28, 2020

The cooling tower pump calculations are completed, the project is bid, the Bell & Gossett pumps scheduled are awarded and installed. There is a noise coming from the pump. The first thing you hear from everyone, “The pump is making noise so it must be cavitating!” Today, the R.L. Deppmann Monday Morning Minutes examines gauge readings to determine the actual available NPSHA.



Gauge Readings Start with a Gauge



To read out a gauge on the cooling tower pump suction, we need a gauge. There is a chance the readings may be less than “0” PSIG so make it a compound gauge. Accuracy is also important so use a grade 2A ½% accurate gauge. The normal cooling tower pump head is typically low, so select the gauge with a lower maximum pressure that still works for the discharge reading. An example would be the Miljoco model P4509LX-004 with a range of 30” to 60 PSI. This will give you a readout in 1” Hg increments on the vacuum side.

How Do I Check NPSH Feet When the Gauge Reads Inches HG?

Conversion of Gauge Pressure/Vacuum to NPSH Available															
PSIG	4	2	0	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
INCHES-HG	NA	NA	0	2	4	6	8	10	12	14	16	18	20	22	24
PSIA	18.7	16.7	14.7	13.7	12.7	11.8	10.8	9.8	8.8	7.8	6.8	5.9	4.9	3.9	2.9
NPSHA	44	39	34	32	30	28	25	23	21	19	16	14	12	9	7

There are plenty of links to equations on the internet but here is a quick chart I made to convert a reading in inches of HG to absolute feet of head. But first there is a correction to think about when you take the reading.

When reading pressure gauges anywhere in the system, you should decide if a [velocity head correction](#) will make a difference. The link will take you to an explanation I made a while ago on this subject.

Good design practice keeps the suction piping velocity low in cooling tower applications. The low velocity should make any velocity head correction readings very low. The example pump from parts 2 and 3 had a 6" suction size and a design of 1000 GPM. Using the formula in the link above, we find the correction to be 1.9 feet. This is added to the NPSHa from above.

Example 1: The Miljoco 4509LX-004 compound gauge reads 8" on the example 6" pump. The chart above shows the 8" HG reading gives us 25 feet NPSHA. The velocity head correction is 1.9 feet. The actual corrected NPSHa is $25 + 1.9$ or about 27 feet.

We could also use the system syzer and a simple subtraction to find the velocity head correction in feet.

Example 2: A gauge on a cooling tower pump with a 10" suction reads 4" HG. The flow is 3000 GPM. What is the reading including the velocity head correction?

Step 1: Go to the electronic system syzer Flow/Pressure Drop tab. Change the temperature to 85°F. Select 10" steel pipe at 3000 GPM.

The screenshot shows the 'Flow/Pressure Drop Relationship' tab. The 'Pipe Size' is set to '10 in' and the 'Pipe Material' is 'Steel Pipe'. The 'Flow Rate' is '3000.00 GPM'. The 'Friction Loss' is '4.04 Feet/100 Feet' and the 'Velocity' is '12.20 Feet/Sec'. A note at the bottom states: 'Steel Pipe thru 24" is Schedule 40' and 'Steel Pipe 30 - 36" is Schedule 30'.

Step 2: Go to the Length/Pressure drop tab. It defaults to 500 feet with no fittings. This is fine for what we are doing here.

The screenshot shows the 'Length/Pressure Drop' tab. The 'Pipe Length (T.E.L.)' is '500.00 Feet'. The 'Friction Loss' is '4.04 Feet/100 Feet' and the 'Total Head Loss' is '20.20 Feet'. On the right side, the 'Pipe Length' is '500.00 Feet' and '152.40 Meters'. The 'Total Head Loss' is displayed in multiple units: '20.20 Feet', '8.74 PSI', '6.16 Meters', '0.60 Bar', and '60.29 kPa'.

Step 3: Go to the NPSHa tab. The height defaults to nothing and that is fine. Notice the NPSHa reads 13.1 feet. Now check the “Include velocity head” button. Notice the NPSHa is now 15.4 feet. The correction is the difference: $15.4 - 13.1 = 2.3$ feet.

The image displays two side-by-side screenshots of the 'NPSHa Calculator' software interface. Both screenshots show the 'NPSHa' tab selected in the top menu bar. The interface includes input fields for 'NPSH Available to Pump', 'Location Elevation', 'Pipe Friction Loss', and 'Height of Dim Z'. In the left screenshot, 'NPSH Available to Pump' is 13.1 feet, 'Location Elevation' is 'Sea Level', 'Pipe Friction Loss' is 20.20 feet, and 'Height of Dim Z' is 0 feet. The 'Include Velocity Head' checkbox is unchecked. In the right screenshot, 'NPSH Available to Pump' is 15.4 feet, 'Location Elevation' is 'Sea Level', 'Pipe Friction Loss' is 20.20 feet, and 'Height of Dim Z' is 0 feet. The 'Include Velocity Head' checkbox is checked.

Step 4: Take the gauge reading of 4” and look at the chart above. The chart indicates 30 feet of NPSHA. Add the 2.3 feet and the corrected NPSHa is 32.3 feet.

In part 5, we will complete this series by looking back at some cooling tower pump suction piping recommendations.

Check out the rest of the Net Positive Suction Head (NPSH) Series:

Part One – [Terms and Definitions](#)

Part Two – [NPSH Safety factors](#)

Part Three – [Calculating NPSH Available](#)



Cleveland | Detroit | Grand Rapids | Saginaw

Deppmann.com | P:800.589.6120 | F:248.354.3763
